

# Theoretical Analysis of Doping Management

Amira Tandirovic Gursel<sup>1</sup>, Parviz Elahi<sup>2</sup>, F. Ömer Ilday<sup>2</sup>, M. Sadettin Özyazıcı<sup>3</sup>

<sup>1</sup>Electrical and Electronics Engineering, Gaziantep University, Gaziantep, 27310, Turkey  
gursel@gantep.edu.tr

<sup>2</sup>Department of Physics, Bilkent University, Ankara, 06800, Turkey  
elahi@fen.bilkent.edu.tr, ilday@bilkent.edu.tr

<sup>3</sup>Electrical and Electronics Engineering, Bahcesehir University, Istanbul, 34353, Turkey  
sadettin.ozyazici@bahcesehir.edu.tr

## Abstract

**Two opposing requirements, such as thermal load and nonlinear effects are important limitations in rapid progress of high-power fiber laser technologies. Thermal effects, which limit the average power, can be minimized by using low-doped, longer gain fibers, whereas presence of nonlinear effects requires use of high-doped, shorter fibers to maximize the peak power. Proposed solution of the problem is the use of varying doping levels along the gain fiber to circumvent to mitigate the trade-off between thermal load and nonlinear effects.**

## 1. Introduction

High- power fiber lasers (HPFL), originally developed for telecom applications [1], have numerous different applications in medicine, remote sensing, material processing etc. due to number of intrinsic advantages, including simplicity of optical cavity construction, high efficiency, excellent beam quality, and micro joule- level energies at high repetition rates that scale up processing speed [3], [7]. Although the pioneering works were limited to sub-W levels [3], strong demand for higher and higher power levels have brought about rapid progress of technology resulted in development of multi-kW ones [10], [18].

A common approach for higher laser efficiency is to increase the dopant concentration which results in a higher absorption coefficient. Concurrently, this causes considerable thermal rise in the fiber core. Heating and beam-distorting effects are critical for high-power lasers [1]. Therefore, there is a great deal of interest in scaling average power along with heat removal and thermal management [12].

With regard to research, it can be said that previous solutions were focused on improvements of pumping diodes [3][5] and pumping technologies as well as fabrication and cooling process of gain fibers at different wavelengths [8][12]. In this context,

important step forward in the evolution of the high gain fibers was introduction of cladding pumping [17]. Although the quantum efficiency double clad fiber lasers (DCFL's) is high, the temperature increase in the fiber core, generated by conversion of around 20% of pumping radiation into heat, will damage the coating material, which adversely affects the laser performance. So, ones more, it is necessary to emphasize importance of quantitatively describing and analyzing of thermal effects which strongly depend of the natural and geometrical properties of the fiber medium, pump beam intensity profile, and the laser cooling method used [12].

There is no doubt that the cooling process is very important but it is also quite certain that the process will be limited along increasing of expected power levels. Therefore, it may be deduced that it is needed to find some additive method to take heat under control. Herein doping management approach [18], revealed by Ilday and colleagues, can be promising method for further research.

This study is theoretical analysis of doping management, according to the thermal conductive equations taking to account natural and geometrical properties of the fiber medium as well as pump beam intensity profile.

## 2. Temperature distribution of double-clad active fibers lasers

Fiber temperature during operation is a 3D boundary value problem with the core acting as a heat source. The inner and outer claddings can be considered as one body since no source is represented in the cladding region resulting in secondary effects of outer cladding that can be ignored. The radial thermal distribution model for double-clad fiber is shown in Figure 1.  $r$  is the radial coordinate and  $\phi$  is the tangential angle. The quantities  $a$  and  $b$  are core cladding radii, respectively [9].  $T_1(r,z)$  and  $T_2(r,z)$  are the temperatures in the core and cladding regions, respectively.

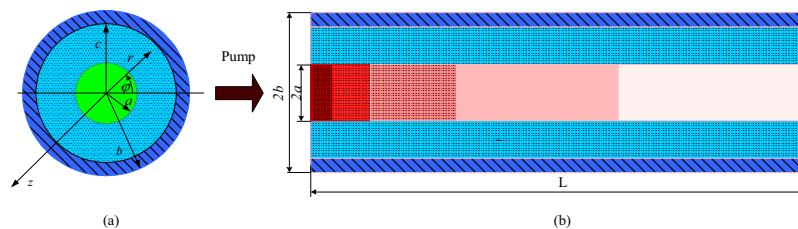


Fig. 1 Geometry of modeled double-clad fiber

The steady-state heat equations for both core and cladding regions are given as follows:

$$\frac{1}{r} \frac{\partial}{\partial r} \left( r \frac{\partial T_1(r,z)}{\partial r} \right) + \frac{\partial^2 T_1(r,z)}{\partial z^2} = -\frac{Q(r,z)}{k_c}; 0 \leq r \leq a \quad (1)$$

$$\frac{1}{r} \frac{\partial}{\partial r} \left( r \frac{\partial T_2(r,z)}{\partial r} \right) + \frac{\partial^2 T_2(r,z)}{\partial z^2} = 0; a \leq r \leq b \quad (2)$$

In (1)  $k_f$  denotes the thermal conductivity of the fiber and the heat density  $Q(r,z)$  as functions of radius and propagation distance. For pumping distribution given by  $P = \xi P_o \exp(-a(z)z)$  heat source density function can be represented as:

$$Q(r,z) = \frac{\xi}{\pi a^2} P_o \exp(-a(z)z) \quad (3)$$

where  $P_o$  denote the pump power,  $a(z)$  is the pump absorption coefficient,  $\xi$  is the fractional thermal load or the conversion coefficient [14].

In (2) the right side of the equation is zero as no source is represented. Temperature functions from (1) and (2) have to be solved using method of separating variables with transformation  $T(r,z) = \varphi(r)\theta(z)$ , taking to account that temperature function has two separable components in radial and axial directions [12][13]. The differential equations to be solved are two separately differential equations with and without source respectively.

$$\frac{1}{r\varphi_1(r)} \frac{\partial}{\partial r} \left( r \frac{\partial \varphi_1(r)}{\partial r} \right) + \frac{1}{\theta_1(z)} \frac{d^2 \theta_1(z)}{dz^2} = -\frac{\xi P_o \alpha(z) \exp(-\alpha(z)z)}{k_f \pi a^2 \varphi_1(r) \theta_1(z)} \quad (4)$$

$$\frac{1}{r\partial \varphi_2} \frac{\partial}{\partial r} \left( r \frac{\partial \varphi_2(r)}{\partial r} \right) + \frac{1}{\theta_2(z)} \frac{d^2 \theta_2(z)}{dz^2} = 0 \quad (5)$$

It is to be notified that both sides of equations (4) and (5) are divided by  $\varphi(r)\theta(z)$ .

As absorption coefficient is variable along of  $z$ , equation (4) is as such insolvable. Because of this, the fiber is considered as system divided into each  $L/n$  length long  $n$  sub-systems along the fiber axis where  $L$  is the length of the fiber. And, for large values of  $n$ , all of that sub-systems act as separately part that absorption coefficient can be treated as constant. It is important to notify that, in terms of both power and temperature, the input of the each sub-system, except the first one, is the output of the previous one. So, pumping distribution of  $i$ -th sub-system, where  $1 \leq i \leq n$  can be represented as:

$$P_i = P_{(i-1)} \exp(-\alpha_i \frac{L}{n}) = P_o \exp(-\frac{L}{n} \sum_{j=1}^i \alpha_j) \quad (6)$$

Taking to account this property, equations (4) and (5) can be rewritten as:

$$\frac{1}{r\varphi_{1i}(r)} \frac{\partial}{\partial r} \left( r \frac{\partial \varphi_{1i}(r)}{\partial r} \right) + \frac{1}{\theta_{1i}(z)} \frac{d^2 \theta_{1i}(z)}{dz^2} = -\frac{\xi P_i \alpha_i \exp(-\alpha_i z_i)}{k_f \pi a^2 \varphi_{1i}(r) \theta_{1i}(z)} \quad (7)$$

$$\frac{1}{r\partial \varphi_{2i}} \frac{\partial}{\partial r} \left( r \frac{\partial \varphi_{2i}(r)}{\partial r} \right) + \frac{1}{\theta_{2i}(z)} \frac{d^2 \theta_{2i}(z)}{dz^2} = 0 \quad (8)$$

where  $z_i = i \frac{L}{n}$ .

For axial parts represented in exponential decay form  $\theta_{1i}(z) = \exp(-\alpha_i z_i)$ ,  $\theta_{2i}(z) = \exp(-\beta_i z_i)$ , and  $\eta_i = \xi P_i \alpha_i / k_f \pi a^2$  equations are transformed into modified zero-order Bessel and zero-order Bessel equations respectively whose representations are given below:

$$\frac{1}{r\varphi_{1i}(r)} \frac{\partial}{\partial r} \left( r \frac{\partial \varphi_{1i}(r)}{\partial r} \right) + \alpha_i^2 = -\frac{\eta_i}{\varphi_{1i}(r)} \quad (9)$$

$$\frac{1}{r\partial \varphi_{2i}(r)} \frac{\partial}{\partial r} \left( r \frac{\partial \varphi_{2i}(r)}{\partial r} \right) + \beta_i^2 = 0 \quad (10)$$

So, solutions for the radial parts of the temperature functions with and without source are:

$$\varphi_{1i} = \alpha_i J_0(\alpha_i r) - a_{2i} Y_0(\alpha_i r) - \frac{\eta_i}{\alpha_i^2} \quad (11)$$

$$\varphi_{2i} = b_{1i} J_0(\beta_i r) - b_{2i} Y_0(\beta_i r) \quad (12)$$

Hence, the temperatures of  $i$ -th sub-system can be represented as:

$$T_{1i}(r, z_i) = \eta_i \left[ A_{1i} J_0(\alpha_i r) - A_{2i} Y_0(\alpha_i r) - \frac{1}{\alpha_i^2} \right] \exp(\alpha_i z_i) + T_c \quad (13)$$

$$T_{2i}(r, z_i) = \eta_i [B_{1i} J_0(\beta_i r) - B_{2i} Y_0(\beta_i r)] \exp(\beta_i z_i) + T_c \quad (14)$$

$A_{1i}$ ,  $A_{2i}$ ,  $B_{1i}$ , and  $B_{2i}$  are arbitrary constants to be determined from boundary conditions given below [10].

$$\partial T_1(r, z_i)|_{r=0} = finite \quad (15)$$

$$T_1(r, z_i)|_{r=a} = T_2(r, z_i)|_{r=a} \quad (16)$$

$$\int_V Q(r, z_i) dV = \int_S k_c \frac{\partial T_2(r, z_i)}{\partial r} \Big|_{r=b} dS \quad (17)$$

$$\frac{\partial T_2(r, z_i)}{\partial r} \Big|_{r=b} = \frac{h}{k_c} (T_c - T_2(r, z_i)|_{r=b}) \quad (18)$$

$k_c$ ,  $T_c$ , and  $h$  are the thermal conductivity, the cooling temperature, and the convective coefficient of the surface, respectively.

From conditions (15) and (16) it is found that  $A_{2i}$  have to be zero as well as  $\alpha_i = \beta_i$ . Hence, relation between  $A_{1i}$ ,  $B_{1i}$ , and  $B_{2i}$  can be expressed as:

$$A_{1i} = B_{1i} - B_{2i} \frac{Y_0(\alpha_i a)}{J_0(\alpha_i a)} + \frac{1}{J_0(\alpha_i a) \alpha_i^2} \quad (19)$$

Relation between  $B_{1i}$ , and  $B_{2i}$  can be obtained introducing the definition for derivative of Bessel function in condition (17)

$$B_{1i} J_1(\alpha_i b) - B_{2i} Y_1(\alpha_i b) = \frac{a^2}{2bK\alpha_i} \quad (20)$$

where  $K = k_c / k_f$ .

From condition (18) it is found that:

$$B_{2i} = \frac{h J_0(\alpha_i b) - k_c \alpha_i J_1(\alpha_i b)}{h Y_0(\alpha_i b) - k_c \alpha_i Y_1(\alpha_i b)} B_{1i} \quad (21)$$

Equations (19), (20), and (21) form an equation set whose solutions are found to be:

$$A_{1i} = \frac{a^2 (J_0(\alpha_i a) - \gamma Y_0(\alpha_i a))}{2bK\alpha_i J_0(\alpha_i a) (J_1(\alpha_i b) - \gamma Y_1(\alpha_i b))} + \frac{1}{\alpha_i^2 J_0(\alpha_i a)} \quad (22)$$

$$B_{1i} = \frac{a^2 \gamma}{2bK\alpha_i (J_1(\alpha_i b) - \gamma Y_1(\alpha_i b))} \quad (23)$$

$$B_{2i} = \frac{a^2 \gamma}{2bK\alpha_i (J_1(\alpha_i b) - \gamma Y_1(\alpha_i b))} \quad (24)$$

where  $\gamma = \frac{h J_0(\alpha_i b) - k_c \alpha_i J_1(\alpha_i b)}{h Y_0(\alpha_i b) - k_c \alpha_i Y_1(\alpha_i b)}$

Finally, using equations (13-14) and (22-24), 2-D analytical solutions for temperature distribution at of core and clad regions respectively, for variable absorption coefficient, are obtained as follows:

$$\begin{aligned} T_{1i}(r, z_i) &= \frac{\xi \alpha_i}{k_f \pi a^2} P_o \exp \left( -\frac{L}{n} \sum_{j=1}^i \alpha_j \right) \left[ \left( \frac{a^2 (J_0(\alpha_i a) - \gamma Y_0(\alpha_i a))}{2bK\alpha_i J_0(\alpha_i a) (J_1(\alpha_i b) - \gamma Y_1(\alpha_i b))} \right. \right. \\ &\quad \left. \left. + \frac{1}{\alpha_i^2 J_0(\alpha_i a)} \right) J_0(\alpha_i r) - \frac{1}{\alpha_i^2} \right] \exp(-\alpha_i z_i) + T_c \end{aligned} \quad (25)$$

$$\begin{aligned} T_{2i}(r, z_i) &= \frac{\xi \alpha_i}{k_f \pi a^2} P_o \exp \left( -\frac{L}{n} \sum_{j=1}^i \alpha_j \right) \left[ \frac{a^2}{2bK\alpha_i (J_1(\alpha_i b) - \gamma Y_1(\alpha_i b))} J_0(\alpha_i r) - \right. \\ &\quad \left. \frac{a^2 \gamma}{2bK\alpha_i (J_1(\alpha_i b) - \gamma Y_1(\alpha_i b))} Y_0(\alpha_i r) \right] \exp(-\alpha_i z_i) + T_c \end{aligned} \quad (26)$$

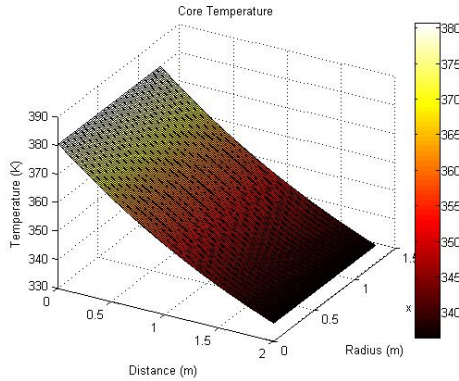
### 3. Results

It can be said that the calculations are divided into 2 parts: verification of the functions for constant absorption coefficient and calculations for variable absorption coefficient. Table 1. shows the parameters used during the calculations.

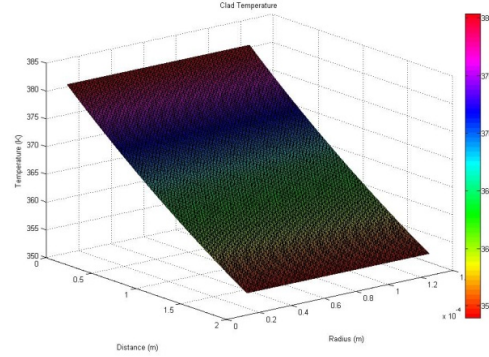
Parameter	Amount	Unit
a	12.5	$\mu\text{m}$
b	125	$\mu\text{m}$
$k_c$	23	W/mK
$P_o$	150	W
$T_c$	300	K
$h_c$	50	W/m <sup>2</sup> K
$k_f$	230	W/mK
L	2	m
n	400	
$\lambda_p$	976	nm
$\lambda_p$	1060	nm

Table1. Parameters used in calculations.

For constant absorption coefficient calculations 3 different absorption coefficients have been used:  $\alpha_1=0.4$ ,  $\alpha_2=0.1$ , and  $\alpha_3=0.01$ . Fig. 2.a and 2.b show the temperature distributions of core and clad along r and z axis.



2.a



2.b

Fig. 2.a-b Illustrations of temperature distributions of core and clad respectively in r-z plane

In order to take more precise information the equations are plotted for both  $r=a$  and  $r=b$ . One of these graphs is shown in Fig.3

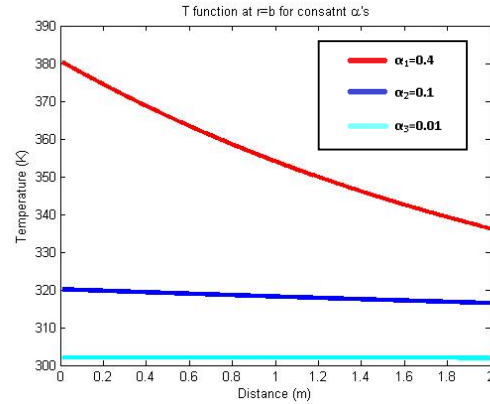


Fig.3 Temperature distribution at  $r=b$

According to Figure 3 it is quite certain that an increase of absorption coefficient cases higher maximum temperature reached at pumping side of the fiber laser. At the same time, higher absorption coefficient provides more significant drop in temperature along the fiber. On this basis, it can be deduced that some increasing absorption function can cause reduction of the temperature along the fiber.

For calculations with variable absorption coefficient 3 different polynomials were used:

$$\alpha_1(z) = -0.0081z^5 + 0.0814z^4 - 0.1628z^3 + 0.1747z^2 - 0.0237z + 0.01 \quad (27)$$

$$\alpha_2(z) = 0.0326z^5 - 0.179z^4 + 0.4036z^3 - 0.5651z^2 + 0.6221z + 0.01 \quad (28)$$

$$\alpha_3(z) = 0.195z + 0.01 \quad (29)$$

Figure 4.a illustrates 3 different increasing absorption coefficient functions given, rise between 0.01 and 0.4, used for temperature calculations which results are represented in Figure 4.b.

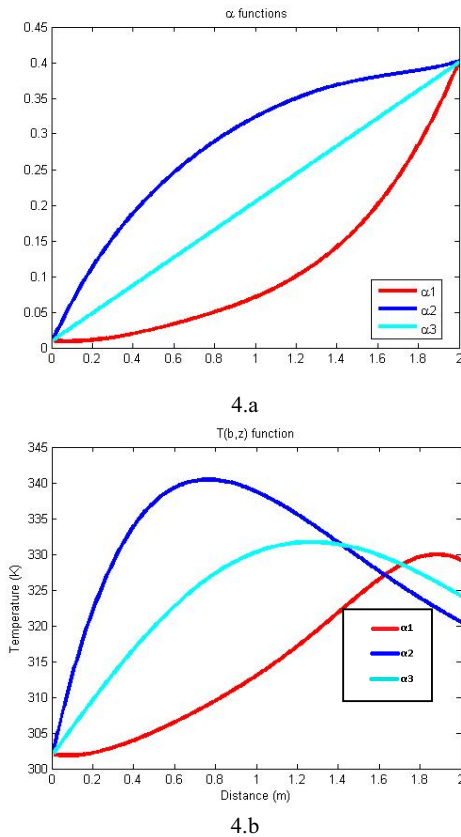


Fig.4.a-b Temperature distributions at  $r=b$  for 3 different polynomials.

As can be seen from Figure 3.b gradual rise of the absorption coefficients results in gradual temperature increase. But, more important, all of the temperature functions with gradually raised absorption coefficient produce considerably smaller temperature rates than constant case, that verify practical results presented by Elahi and colleagues [18]. Additionally, the best results are achieved for the first absorption coefficient function.

#### 4. Conclusion

In this work, at first we have constructed a heat dissipation model for double-clad fiber lasers with top-hat pump beam with cooling at the outer cladding surface and analytically solved 3-D heat transfer functions for variable absorption coefficient. According to analysis, we have presented graphs for both different constant and different variable absorption coefficients. The calculations not only verify experimentally proved postulate of Elahi and colleagues but also show that gradually rise of absorption coefficient causes remarkable reduction in temperatures at core and clad of the fiber laser and may be lifesaver of devastating temperatures at fiber cores. The numerical results also show that the third dimension in thermal analysis of any type of high-power fiber lasers cannot be ignored. Moreover, it can be introduced as active part of thermal control.

#### 5. References

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